

# PATENT SPECIFICATION

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DRAWINGS ATTACHED



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## (54) SEPARATION OF VOLATILE CONSTITUENTS FROM POLYMER COMPOSITIONS

- (71) We, UNION CARBIDE CORPORATION, a Corporation organised under the laws of the State of New York, United States of America, of 270 Park Avenue, New York, State of New York, United States of America, do hereby declare the invention, for which we pray that a patent may be granted to us, and the method by which it is to be performed, to be particularly described in and by the following statement:—
- This invention relates to an apparatus and a method for separating volatile constituents from a liquid composition containing polymer and volatile constituents.
- In the preparation of polymer as in bulk and solution polymerization or by other conventional methods, considerable amounts of starting materials, such as unreacted monomer or solvent remain admixed or entrained in the polymer product. This contamination of polymer is undesirable because of adverse effects on polymer properties as is well known in the art. A common method of separating the polymer from such fluid compositions is the devolatilization thereof. The composition is heated and introduced into a low pressure chamber to flash vaporize solvent and other volatiles causing foaming of the composition. However, a major difficulty with this method is that considerable vapor is entrapped in the foam and remains with the product. In addition, the cooling caused by vaporization so increases the viscosity of the product that it is difficult to remove the polymer from the flash chamber and, moreover at about 90% solids, the polymer solution tends to adhere to the chamber walls blocking the system.
- The fluid composition can be further heated to offset the above problems; however, heating the composition to compensate for the cooling due to vaporization or to assist the flowability thereof can result in polymer degradation or other undesirable polymer formation.
- Accordingly, it is the object of this invention to provide an apparatus for removing volatile constituents from a viscous fluid polymer composition to obtain a liquid polymer product of substantially greater than 90% solids, which apparatus can readily pump the viscous product to recovery or further processing.
- The present invention provides a devolatilization apparatus comprising at least one helical screw rotatably mounted in a barrel in close clearance therewith, said screw having a rearward end and a forward end and adapted to connect at the rearward end with rotating means therefor, at least one vapor vent situated in said barrel proximate said rearward end, adapted to connect with evacuating means, an extruder discharge port situated in said barrel proximate said forward end and a feed solution inlet port situated in said barrel between said vapor port and said discharge port, at least a portion of said screw between said feed port and discharge port tapering toward said discharge end.
- The present invention also provides a method of separating volatile constituents from a liquid composition containing polymers and volatile constituents which method comprises heating said composition at a given pressure to a temperature sufficient to vaporize volatile constituents thereof at a lower pressure or to a temperature sufficient to boil said composition at said given pressure, introducing said composition to the threaded screw of an extruder, at a position intermediate of a vapor vent and tapered screw section having progressively reduced thread maintaining said lower pressure in the chamber of said extruder to vaporize volatile constituents from said composition as it enters therein to foam or further foam said composition and effect substantial release of the volatile constituents therefrom, rotating the screw to advance the foam composition along the thread grooves to progressively compress and compact the foam composition and effect the further release of volatile constituents therefrom and passing the devolatilized and concentrated polymer

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composition from said extruder while separating the released volatile constituents by passing back through the polymer composition to the vapor vent.

Two embodiments of the invention will now be described in conjunction with the accompanying drawings, in which:

Figure 1 is a sectional elevation view of an apparatus suitable for carrying out the devolatilization process of the present invention, and

Figure 2 is a sectional elevation view of another embodiment of an apparatus suitable for carrying out the process of the present invention.

Referring now to the accompanying drawings, extruder screw 10 is rotatably mounted in extruder barrel 12 as illustrated in Figure 1. The screw 10 is driven by means (not shown) connected to the screw 10 by means of shaft 14. The extruder barrel 12 is maintained at reduced pressure by suitable evacuating means (not shown) connected to the extruder barrel by way of rear vent 28. A liquid polymer composition (not shown) heated to a suitable devolatilization temperature is introduced to the extruder barrel 12 through inlet port 26 whereupon the composition flash devolatilizes, foams and is urged along the screw 10 toward tapered section 22 for compression and further devolatilization. The extruder screw 10 which has threads 18 separated by thread grooves 16 tapers from its rearward end toward the discharge section 24 as shown in Figure 1. The tapered section 22 is characterized by progressively reduced thread diameter and correspondingly reduced groove or inner diameter. The extruder barrel 12 is sized to conform to the shape of the screw 10 and the screw is mounted in working proximity, i.e. in close clearance with the walls of the extruder barrel. The discharge section 24 and the surrounding barrel 12 extend at a relatively constant diameter to provide an ample pumping pressure for the devolatilized polymer as it is conveyed toward the discharge port 30. The tapered section 22 preferably runs full along at least a part of its length to provide a buffer zone to dampen surging of the solution in the apparatus and provide relatively smooth product discharge. The devolatilized and concentrated polymer solution is discharged through discharge port 30. The barrel 12 as indicated above is contoured to the profile of the screw as shown in Figure 1 to assure virtually complete product removal.

In another embodiment of the invention, a plurality of tapering screws can be employed as shown, for example, in Figure 2. Twin tapering screws 34 and 36 are rotatably mounted in extruder barrel 32 in close proximity with one another. Screw 34 has threads 38 separated by thread grooves 40,

and screw 36 has threads 42 separated by thread grooves 44. The extruder barrel 12, as shown in Figure 2, is tapered toward the discharge end thereof to follow closely the profile of the screws 34 and 36 so that the threads 38 and 42 thereof sweep the inner surfaces of the barrel 12 substantially clean of polymer solution. Polymer feed solution is fed to the barrel 12 through inlet port 46 foamed, compressed and devolatilized as it is advanced along the tapering screws and is discharged at product discharge port 50. A vacuum pump (not shown) serves to maintain the barrel 12 at reduced pressure as well as drawoff vapors released from the solution being devolatilized by way of rear vent 48.

By the apparatus of the present invention a liquid composition as dilute as 50% by weight polymer can be processed to substantially solvent-free polymer having less than 1% and frequently less than .05% by weight of residual solvent including monomer or other volatile therein. For example, polystyrene solution containing 50% by weight of the polymer in unreacted monomer can be processed to 99.9% by weight of the polymer or more.

The fluid polymer composition can be composed of virtually any polymeric material such as polystyrene, the polyolefins such as polyethylene and polypropylene or vinyl polymers dissolved in a suitable solvent such as its monomer, or inert organic liquids such as benzene, toluene, heptane, and acetone.

The polymer composition can be fed to the devolatilizing apparatus of the present invention at varying rates depending on such factors as the nature of the feed materials, the feed temperature, pressure in the extruder barrel of the apparatus, RPM of the screw or screws or size of the equipment. The example appearing hereinbelow serves as an illustration of a combination of such factors which can be readily determined by the skilled practitioner in accordance with process demands.

The fluid composition is fed to the apparatus of the invention at temperature sufficient to cause vigorous devolatilization thereof when the feed enters the extruder barrel but below the temperature at which the particular solution components degrade or are otherwise adversely affected. The solution can be maintained at a pressure sufficiently high to prevent boiling thereof in the feed lines by throttle valves, for example, mounted in the lines adjacent to the apparatus. However, the solution is preferably heated to boiling before being fed to the apparatus of the invention for devolatilization and concentration thereof. For example, the solution to be concentrated is passed through a heat exchanger, where it

is boiled and discharged as a foamy mass into the apparatus of the invention, which is usually operated under reduced pressure. The vapors from the incoming boiling solution, joined by additional vapors generated by flashing and mechanical shearing of the solution in the apparatus then proceed in a helical path rearward along the flights of the screw toward the vapor vent of the apparatus. As the viscous polymer is conveyed by drag flow toward the discharge port (prior to densification), new surface is exposed for additional vaporization. This latter source of vapor, continues until the combined effects of back pressure and of the reduction in cross sectional area cause the flights to run full. Beyond this point there is substantially no further vapor release.

The pressure in the extruder barrel is maintained below the vapor pressure of the feed solution and preferably well below the feed pressure to provide a substantial pressure drop and flash vaporization of volatiles such as the solvent or solvents thereof, with resultant vigorous foaming of the solution. The temperature within the barrel is preferably sufficiently high to maintain the solution product in a liquid state as well as vaporize the solvent component. The operating temperature of the barrel is determined by diverse factors, for example, by its maintained pressure and the thermal properties of the feed solution which upon entering expands and cools.

Although the pressure in the extruder barrel varies depending upon the particular solvents or other volatiles being vaporized, it has been found that pressures in the range of from about 10 to about 760 mm Hg or above are suitable; the lower end of the range being preferred particularly from 10 to 300 mm Hg.

One or more vapor vents are situated in the apparatus upstream from the inlet port of the polymer feed solution rear vents, in order to prevent loss of polymer out the vent. Thus the entering polymer solution is immediately conveyed downstream away from the rear vent by the screw or screws while the released vapors can flow upstream or countercurrent to the polymer in a helical or other rearward path and out the rear vent under the influence of a vacuum pump.

As indicated, a conventional vacuum pump or other suitable evacuating means, connected, for example, to the apparatus of the invention by way of the vapor vent above, can be conveniently employed in the present invention. A condenser can be

connected to the vacuum pump, e.g., for recovery of the stripped volatiles. However, when a low boiling solution is fed to the chamber, for example, under high temperature and pressure, evacuating means can appropriately be dispensed with in accordance with process requirements.

The extruder screw and barrel are preferably made of rigid material such as metal for example stainless steel or other suitable metal. The threads of the screw can take various shapes as desired and can vary angular to rounded. The threads can be of uniform distances from one another or different distances for example they can become more closely spaced going from the rearward to the extrusion end of the screw. The screw moreover can have more than one tapering zone as suitable for the given application. It is desirable that at least the last such tapered zone of the screw be in close contact with the extruder barrel and taper from rearward to forward end of the screw.

Where more than one screw is employed in the extruder barrel, the screws can intermesh or be mounted in close proximity without intermeshing. Moreover the screws can co-rotate or counter rotate as desired. Preferably the screws co-rotate and closely intermesh, so that the threads thereof wipe the surfaces of each other as well as the barrel surfaces.

The screw or screws can be rotated at any suitable speed of up to about 300 RPM or more in accordance with process and mechanical requirements.

The following Example is intended as an illustration of the invention.

#### EXAMPLE

A solution of polystyrene in its monomer was devolatilized in an apparatus similar to that shown in Figure 1. The screw was 27 inches long having a 12 inch input section connected to a 12 inch tapering section and a 3 inch discharge section, extending from the smaller end of the tapering section. The screw had a crest diameter of 7.5 inches and a root diameter of about 3.7 inches at the input section which tapered to a crest diameter of about 1.5 inches and a root diameter of 1.0 inch at the above 3 inch section. The screw threads had a thickness of 1/8 inch near the crest thereof tapering to 2 inches thick at the base thereof. The thread separation varied from 3 inches at the larger end to 1 inch at the smaller end thereof. Examples were run as indicated in the following table.

TABLE

5	Run	Feed Rate lbs/hr.	RPM	Extruder Barrel		% Polystyrene in Feed	% Polystyrene in Product	Product Rate lbs/hr.
				Feed Temperature °C.	Pressure mmHg.			
	1	216.0	66	190	100	53.5	90.7	119.0
	2	106.0	88	194	100	67.8	98.4	69.2
	3	43.5	84	193	100	63.7	99.2	29.4

Thus it is apparent that the apparatus of the invention serves to provide substantially volatile-free polymer. The per cent polymer in the product can be raised by adjustments of the tabulated variables such as lowering the barrel pressure or increasing the temperature of the feed or other means such as increasing the size of the apparatus components, as can be readily determined by the skilled practitioner for a given polymer composition, to produce a product of up to 99.9% polymer or more. Moreover, the polymer product can, where suitable, be reprocessed i.e., subjected to flashing and compression two or more times.

It will be recognized that the apparatus of the present invention can be used singly in devolatilization systems or with one or more other such tapering screw devolatilizers in series as suitable for the desired application. Moreover, the screw apparatus of the present invention can be used in connection with a flash chamber which feeds its product into the screw apparatus and furthermore the extruder screw of the present invention can also be employed with an extruder die of various shapes and size so that the effluent having been devolatilized may immediately be extruded into a desired form. In addition, the devolatilizer of the present invention can be linked in series with another concentrator including a conventional milling stage to obtain virtually pure polymer, such as, for example, a twin screw mill well known in the art.

#### WHAT WE CLAIM IS:—

1. A devolatilization apparatus comprising at least one helical screw rotatably mounted in a barrel in close clearance therewith, said screw having a rearward end and a forward end and adapted to connect at the rearward end with rotating means therefor, at least one vapor vent situated in said barrel proximate said rearward end, adapted to connect with evacuating means, an ex-

truder discharge port situated in said barrel proximate said forward end and a feed solution inlet port situated in said barrel between said vapor port and said discharge port, at least a portion of said screw between said feed port and discharge port tapering toward said discharge end.

2. An apparatus as claimed in claim 1 having twin helical screws.

3. An apparatus as claimed in claim 1 or claim 2 having a feed solution boiling stage up stream of the feed solution inlet port.

4. An apparatus as claimed in any one of claims 1, 2 and 3 having a flash chamber up stream of the feed solution inlet port.

5. A devolatilization system having a plurality of the apparatuses of claims 1 to 4 in communication.

6. A devolatilization apparatus as claimed in any one of claims 1 to 5 having two tapering screws mounted in close proximity with one another in an extruder barrel, said screws being in close proximity with the inside surface of said barrel.

7. An apparatus as claimed in claim 6 wherein said screws intermesh and co-rotate.

8. An apparatus as claimed in any one of the preceding claims wherein the pitch of the screw or screws is reduced between the feed port and the discharge port.

9. A devolatilization apparatus substantially as hereinbefore described with reference to Figure 1 or Figure 2 of the accompanying drawings.

10. A devolatilization apparatus substantially as hereinbefore described with reference to the specific Example.

11. A method of separating volatile constituents from a liquid composition containing polymers and volatile constituents which method comprises heating said composition at a given pressure to a temperature sufficient to vaporize volatile constituents thereof at a lower pressure or to a temperature

- 5 sufficient to boil said composition at said  
given pressure, introducing said composition  
to the threaded screw of an extruder, at a  
position intermediate of a vapor vent and  
5 tapered screw section having progressively  
reduced thread, maintaining said lower pres-  
sure in the chamber of said extruder to  
vaporize volatile constituents from said com-  
position as it enters therein to foam or  
10 further foam said composition and effect  
substantial release of the volatile constituents  
therefrom, rotating the screw to advance the  
foam composition along the thread grooves  
to progressively compress and compact the  
15 foam composition and effect the further re-  
lease of volatile constituents therefrom and  
passing the devolatilized and concentrated  
polymer composition from said extruder  
while separating the released volatile con-  
stituent by passing back through the polymer 20  
composition to the vapor vent.
12. A method as claimed in claim 11  
substantially as hereinbefore described in  
the specific Example.
13. A liquid polymer product of greater 25  
than 90% solids when obtained from an  
apparatus as claimed in any one of claims  
1 to 10.
14. A liquid polymer product of greater  
than 90% solids when obtained by a method 30  
as claimed in claim 11 or claim 12.

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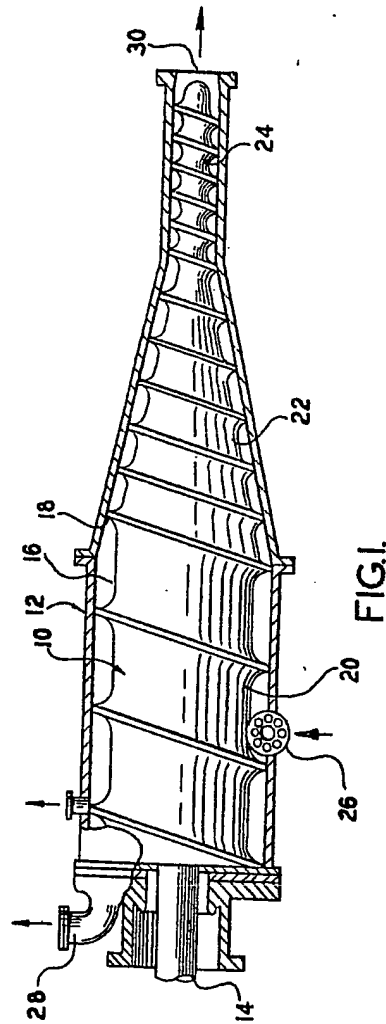
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COMPLETE SPECIFICATION

2 SHEETS

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Sheet 1



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